



Complete range 80 to 4000 kW

HFC-refrigerant free

Hot water source from 110 to 80°C

COPr up to 0.78

16LJ01-03 16LJ-F11-82

Nominal cooling capacity 83-3956 kW

The Carrier 16LJ & 16LJ-F single-effect absorption chillers are designed to provide chilled water from waste heat sources generated from industrial processes and cogeneration systems.

Carrier absorption chillers allow diversification of critical cooling requirements. Critical cooling loads are met with minimal electrical power input.

They allow smaller emergency generators compared to an electrical driven chiller.

The units are ozone-safe and CFC-free. Cooling requirements are met without chlorine-based refrigerants.

They reduce the contribution to global warming and minimise the global impact by greatly reducing electricity consumption and production of greenhouse gases.

The solution inhibitor has no impact on the environment.

An absorption chiller does not utilise mechanical moving parts, and this leads to quiet, vibration-free operation.

The use of high-efficiency heat transfer surface has reduced the space required for installation of the absorption chiller, resulting in a smaller footprint.

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PHYSICAL DATA

16LJ/16LJ-F			LJ		LJ-F									
Size		01	02	03	11	12	13	14	21	22	23	24	31	32
Capacity	kW	83	131	166	264	316	387	475	545	633	738	844	949	1055
Chilled water system*			~			~		~		`	~			
Flow rate	l/sec	3.58	5.64	7.14	12.6	15.1	18.5	22.7	26	30.3	35.3	40.3	45.3	50.3
Pressure drop	kPa	73	60	60	72.2	78.4	48.5	52.9	46.8	50.2	102	105	104	106
Connection(ANSI)	inch	2	2 1/2	2 1/2	3	3	4	4	5	5	5	5	6	6
Retention volume	m ³	0.06	0.08	0.08	0.11	0.13	0.15	0.17	0.22	0.25	0.28	0.30	0.35	0.38
Cooling water system*										`				
Flow rate	l/sec	5.4	8.5	10.8	20.8	25	30.6	37.5	43.1	50	58.3	66.7	75	83.3
Pressure drop	kPa	23	16	15	78.8	81.8	86.6	95.4	89.1	93.4	58.4	62.5	49.8	51.6
Connection(ANSI)	inch	3	4	4	5	5	5	5	6	6	8	8	8	8
Retention volume	m ³	0.13	0.18	0.23	0.33	0.37	0.40	0.45	0.58	0.63	0.69	0.76	0.98	1.05
Hot water system*									,	,		,		
Flow rate	l/sec	3.28	5.17	6.56	8.4	10.1	12.3	15.1	17.3	20.1	23.4	26.8	30.1	33.5
Pressure drop	kPa	58	41	41	24.7	26.4	65.6	72.8	31.5	32.5	22.0	22.1	22.4	22.3
Connection(ANSI)	inch	2	2 1/2	2 1/2	4	4	4	4	5	5	6	6	6	6
Retention volume	m ³	0.04	0.04	0.07	0.07	0.08	0.09	0.10	0.13	0.14	0.15	0.17	0.21	0.22
Rupture disk connection	inch	2	2	2	2	2	2	2	2	2	2	2	2	2
Dimensions														
Length (L)	mm	1745	2450	2450	2 640	2 640	3 650	3 650	3 690	3 690	4 770	4 770	5 300	5 300
Height (H)	mm	2115	2115	2115	2 430	2 430	2 430	2 430	2 600	2 600	2 600	2 600	2 840	2 840
Width (W)	mm	1255	1255	1435	1 400	1 400	1 400	1 400	1 500	1 500	1 500	1 500	1 580	1 580
Tube removal	mm	900	1350	1350	2 400	2 400	3 400	3 400	3 400	3 400	4 500	4 500	4 500	4 500
Weight														
Operation weight	kg	2070	2680	3150	4 000	4 200	5 200	5 500	6 600	6 900	8 100	8 600	10 500	11 000
Max shipping weight	kg	1820	2380	2720	3 500	3 600	4 500	4 700	5 600	5 900	7 000	7 300	9 000	9 300
Shipping method	u	1	1	1	1	1	1	1	1	1	1	1	1	1
Power supply	V-ph-Hz	4	100-3-5	o					40	0-3-50				
Apparent power	kVA	3.1	3.1	3.1	5.0	5.0	5.0	6.8	6.9	6.9	6.9	6.9	10.5	10.5
Total electric current	Α	4.8	4.8	4.8	7.5	7.5	7.5	10.2	10.3	10.3	10.3	10.3	15.5	15.5
Absorbent pump N°1, power input	kW	0.75	0.75	0.75	1.1	1.1	1.1	2.2	2.2	2.2	2.2	2.2	3.0	3.0
Absorbent pump N°1, electric current	Α	2.2	2.2	2.2	2.8	2.8	2.8	5.5	5.5	5.5	5.5	5.5	7.5	7.5
Absorbent pump N°2, power input	kW	/	1	/	0.3	0.3	0.3	0.3	0.4	0.4	0.4	0.4	1.5	1.5
Absorbent pump N°2, electric current	Α	1	1	/	1.4	1.4	1.4	1.4	1.5	1.5	1.5	1.5	4.7	4.7
Refrigerent pump, power input	kW	0.2	0.2	0.2	0.2	0.2	0.2	0.2	0.2	0.2	0.2	0.2	0.2	0.2
Refrigerent pump, electric current	Α	0.7	0.7	0.7	1.3	1.3	1.3	1.3	1.3	1.3	1.3	1.3	1.3	1.3
Purge pump, power input	kW	0.4	0.4	0.4	0.4	0.4	0.4	0.4	0.4	0.4	0.4	0.4	0.4	0.4
Purge pump, electric current	Α	1.1	1.1	1.1	1.15	1.15	1.15	1.15	1.15	1.15	1.15	1.15	1.15	1.15
PD cell heater	kW	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038
Control circuit	kW	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3

Condition for LJ

12,2/6,7 °C (Fouling Factor = 0.0176 m2°C/kW) 29.4/38.4°C (Fouling Factor = 0.044 m2°C/kW) 95/86°C (Fouling Factor = 0.0176 m2°C/kW) 12/7 °C (Fouling Factor = 0.018 m2°C/kW) 29.4/36.3°C (Fouling Factor = 0.044 m2°C/kW) 90/80°C (Fouling Factor = 0.018 m2°C/kW)

Notes: These performance data are provided to support early design activity. For selection outside ARI operating conditions, contact Carrier

Condition for LJ-F



PHYSICAL DATA

16LJ-F								LJ-F						
Size		41	42	51	52	53	61	62	63	71	72	73	81	82
Capacity	kW	1 178	1 319	1 477	1 653	1 846	2 110	2 373	2 637	2 901	3 165	3 428	3 692	3 956
Chilled water system*														
Flow rate	l/sec	56.4	63.1	70.6	78.9	88.3	100.8	113.3	126.1	138.6	151.1	163.9	176.4	188.9
Pressure drop	kPa	102	88.5	74.3	37.4	49.3	95.6	45.9	59.9	114	50.7	62.7	50.8	61.7
Connection(ANSI)	inch	8	8	8	8	8	10	10	10	12	12	12	14	14
Retention volume	m³	0.49	0.56	0.70	0.77	0.83	1.06	1.13	1.21	1.43	1.53	1.63	1.82	1.94
Cooling water system*														
Flow rate	l/sec	93.1	104.2	116.7	130.6	145.8	166.7	187.5	208.3	229.2	250	270.8	291.7	312.5
Pressure drop	kPa	52.8	55.4	94.4	128	43.1	78.1	105	70.6	45.6	57.4	70.8	59.2	71.4
Connection(ANSI)	inch	10	10	12	12	12	14	14	14	16	16	16	16	16
Retention volume	m³	1.31	1.41	1.97	2.13	2.27	2.87	3.05	3.23	3.79	4.02	4.23	4.75	5.10
Hot water system*														
Flow rate	l/sec	37.4	41.8	46.8	52.4	58.5	66.9	75.2	83.6	91.9	101	109	117	126
Pressure drop	kPa	21.7	22.1	63.8	28.6	37.8	27.2	36.4	47.5	37.9	47.9	59.2	49.3	59.8
Connection(ANSI)	inch	8	8	8	8	8	10	10	10	10	10	10	10	10
Retention volume	m ³	0.29	0.32	0.35	0.37	0.40	0.69	0.72	0.76	0.82	0.86	0.90	0.99	1.03
Rupture disk connection	inch	2	2	2	2	2	2	2	2	2	2	2	2	2
Dimensions														
Length (L)	mm	5 330	5 330	5 500	5 950	6 480	6 710	7 210	8 230	7 230	8 220	8 220	8 320	8 320
Height (H)	mm	3 080	3 080	3 450	3 450	3 450	3 680	3 680	3 680	4 000	4 000	4 000	4 180	4 180
Width (W)	mm	1 690	1 690	2 000	2 000	2 000	2 230	2 230	2 230	2 730	2 730	2 730	3 010	3 010
Tube removal	mm	4 500	4 500	4 600	5 200	5 700	5 200	5 700	6 200	5 700	6 200	6 700	6 200	6 700
Weight														
Operation weight	kg	13 000	13 600	18 400	20 000	21 400	28 300	30 300	32 400	38 700	41 200	43 700		49 600
Max shipping weight	kg	10 900	11 300	15 400	16 600	17 900	11 500	12 200	13 100	16 000	17 000		19 000	19 900
Shipping method	u	1	1	1	1	1	2	2	2	2	2	2	2	2
Power supply	V-ph-Hz							400-3-50		1				
Apparent power	kVA	10.6	10.6	10.6	10.6	10.8	18.7	18.7	18.7	24.2	24.2	25.6	25.6	25.6
Total electric current	Α	15.6	15.6	15.6	15.6	15.9	27.4	27.4	27.4	35.3	35.3	37.4	37.4	37.4
Absorbent pump N°1, power input	kW	3.0	3.0	3.0	3.0	3.0	7.5	7.5	7.5	7.5	7.5	7.5	7.5	7.5
Absorbent pump N°1, electric current	Α	7.5	7.5	7.5	7.5	7.5	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0
Absorbent pump N°2, power input	kW	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	3.7	3.7	3.7	3.7	3.7
Absorbent pump N°2, electric current	Α	4.7	4.7	4.7	4.7	5.0	5.0	5.0	5.0	11.0	11.0	11.0	11.0	11.0
Refrigerent pump, power input	kW	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.75	0.75	1.2	1.2	1.2
Refrigerent pump, electric current	Α	1.4	1.4	1.4	1.4	1.4	1.4	1.4	1.4	2.5	2.5	4.6	4.6	4.6
Purge pump, power input	kW	0.4	0.4	0.4	0.4	0.4	0.4	0.4	0.4	0.75	0.75	0.75	0.75	0.75
Purge pump, electric current	Α	1.15	1.15	1.15	1.15	1.15	1.15	1.15	1.15	1.9	1.9	1.9	1.9	1.9
PD cell heater	kW	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038	0.038
Control circuit	kW	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3

^{*} Condition for LJ-F 12/7 °C (Fouling Factor = 0.018 m2°C/kW) 29.4/36.3°C (Fouling Factor = 0.044 m2°C/kW) 90/80°C (Fouling Factor = 0.018 m2°C/kW)

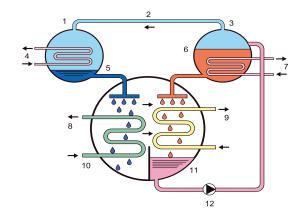
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THE ABSORPTION CYCLE

The absorption cooling cycle, like the mechanical vapour compression refrigeration cycle, utilizes the latent heat of evaporation of a refrigerant to remove heat from the entering chilled water. Vapour compression refrigeration systems use a chlorine-based refrigerant and a compressor to transport the refrigerant vapour to be condensed in the condenser. The absorption cycle, however, uses water as the refrigerant and an absorbent lithium bromide solution to absorb the vaporised refrigerant. Heat is then applied to the solution to release the refrigerant vapour from the absorbent. The refrigerant vapour is then condensed in the condenser.

The basic single-effect absorption cycle (see Figure 1) includes generator, condenser, evaporator and absorber with refrigerant (liquid) and lithium bromide as the working solutions. The generator utilizes a heat source (steam or hot water) to vaporise the diluted lithium bromide solution. The water vapour that is released travels to the condenser where it is condensed back into a liquid, transferring the heat to the cooling tower water. Once condensed, the liquid refrigerant is distributed over the evaporator tubes, removing the heat from the chilled water and vaporising the liquid refrigerant. The concentrated lithium bromide solution from the generator passes into the absorber, absorbs the refrigerant vapour solution from the evaporator and dilutes itself. The diluted lithium bromide solution is then pumped back to the generator where the cycle is started again.

Figure 1 - Simplified absorption cycle

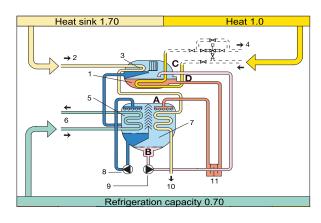


Legend

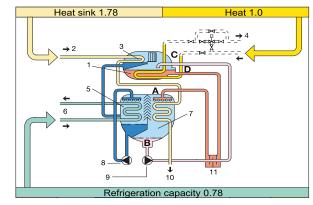
- Condenser
- Refrigerant vapour
- Generator Cooling water
- Liquid refrigerant Concentrated solution
- Heat source
- Chilled water Cooling wate
- 10 Evaporator
- Absorber
- Absorbent pump

Cooling cycle schematic

LJ 01/02/03



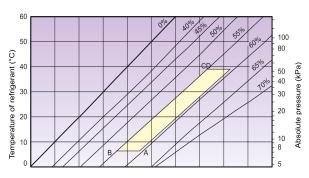
LJF 11-82



Legend

- Generator
- Cooling water
- 3 Condenser Hot water
- Evaporator
- Chilled water
- Absorber
- Refrigerant pump
- Absordent pump

- 10. Heat exchanger
- 11. Cooling water
- Concentrated solution 12.
- 13. Diluted solution 14. Liquid solution
- 15. Refrigerant vapour
- 16. Cooling water
- 17. Chilled water
- 18. Hot water



Temperature of absorbent (°C)



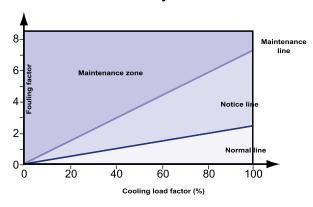
FEATURES AND ADVANTAGES

Expert self-diagnosis function

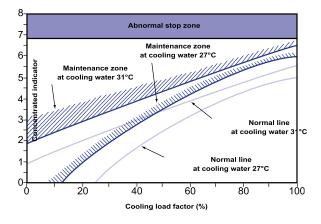
The expert function is provided to monitor operating conditions, predict chiller information and maintain stable operation.

Predictive maintenance information

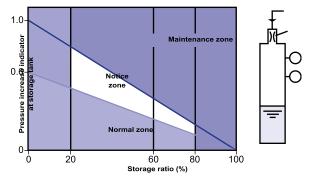
Graph 1 - Fouling of heat transfer tubes in cooling water system



Graph 2 - Tend of absorbent concentration



Graph 3 - Vacuum condition monitoring



Legend

- 1. Storage tank
- 2. Diluted solution
- 3. Purge nozzle
- Pd cell
- Pressure sensor

Control system

- The Carrier control system surpasses other proportional only control systems available today. The digital PID (proportional plus integral plus derivative) control maximises unit performance by maintaining a ±0.5 K variance in leaving chilled-water temperature from the set-point. Proportional controls can typically only maintain a ±1 K variance from the set-point. The controller's innovative design also incorporates the ability to start and stop the system chilled/hot and cooling water pumps. During shutdown these pumps are sequenced to ensure a complete dilution cycle
- The leaving chilled-water temperature is measured every five seconds and steam input is changed according to the gradient of the leaving chilled-water temperature curve. System temperatures, set-points, and operational records are displayed along with indicator lights for the chiller and pumps.
- The Carrier control system offers its users selfdiagnostics by constantly monitoring the chiller status and will automatically shut the chiller down if a fault occurs. The cause of shutdown will be retained in the memory and can be displayed for immediate operator review. The controller's memory will also retain and display the cause of the last three system fault conditions. This method of retaining fault conditions is extremely useful for maintaining an accurate



FEATURES AND ADVANTAGES

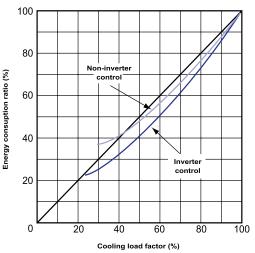
Fast digital PID control

The introduction of new digital PID control stabilises the chilled/hot water temperature with high accuracy. It quickly responds to the load fluctuation and supplies stable chilled/hot water temperature. It is suitable for air-conditioning intelligent buildings which require sophisticated control.

Saving energy with the inverter (option)

Balancing the load and flow rate with the absorbent pump's inverter control enables efficient and energy-saving operation. As a result, it reduces input energy and electric power consumption. Running cost is decreased by 5% compared to non-inverter control.

Graph 4 - Running cost curve



Notes

- 1. Chilled water leaving temperature 7°C constant
- 2. Cooling water entering temperature:

Load factor (%)	Temperature (°C)						
100	32						
50	27						
30	25						

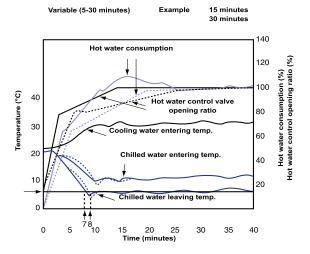
Purge system

The high-performance purge system maintains the required operating pressure, preserves chiller performance characteristics, minimises chiller maintenance to one purge operation per season (for year-round operation).

Hot-water valve opening control

- At the start-up, the opening angle of the hot-water control valve is controlled in three stages, reducing the amount of hot water and the time needed to reach the desired level, compared with the previous model.
- Adjusting the opening speed of the hot-water control valve at the second and third stage, it is possible to set up the most suitable conditions for the site auxiliary equipment.

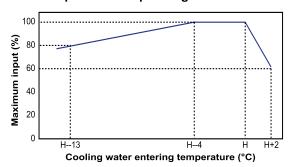
Graph 5 - Hot water valve opening control



Expansion of safe operating zone

- This ensures quick response to rapid changes and maintains stable operation.
- The safe operating zone is between 19 °C and 34 °C cooling water temperature (for a nominal cooling water entering temperature of 32 °C).

Graph 6 - Safe operating zone chart



Crystallisation protection

A microprocessor monitors the absorbent concentration. Steam supply is stopped, and the unit is returned to normal operation, when the concentration is over a certain limit, to prevent the crystallisation of absorbent